



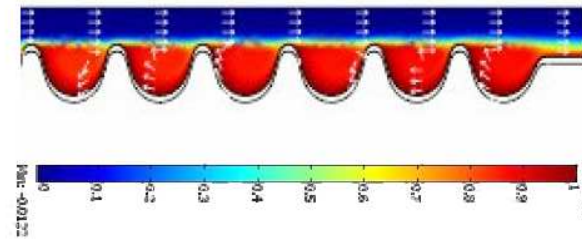
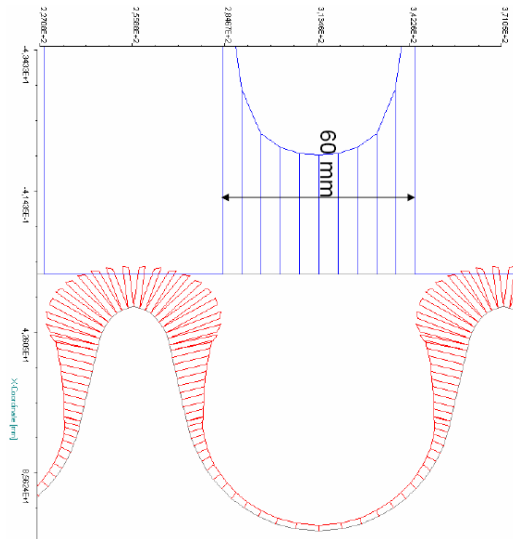
Shape Influence on Electropolishing (Single-Cell Cavities)

*COMSOL modeling
TESLA, RE-ILC and LL-ILC shapes*

Outline

- Chemical Modeling
- Modeling Hypothesis
- Equations - Diffusion Coefficient
- Better electropolishing understanding on **1-cell cavity**
 - 2D Horizontal EP
 - Difference between beam tubes and equator
 - Comparison between different shapes (TESLA, RE and LL)
 - How to obtain an uniform EP ?

Chemical Modeling



- **DESY (ELSYCA)**

EP on Multicell

No fluid dynamics, No Acid properties

Only Current density

Cathode: mask and profile effects

- **FermiLab (COMSOL)**

BCP on Multicell

Fluid dynamics

Temperature and Nb^{5+} concentration

- **Saclay (COMSOL)**

EP on single cell

Fluid dynamics + Convection-Diffusion

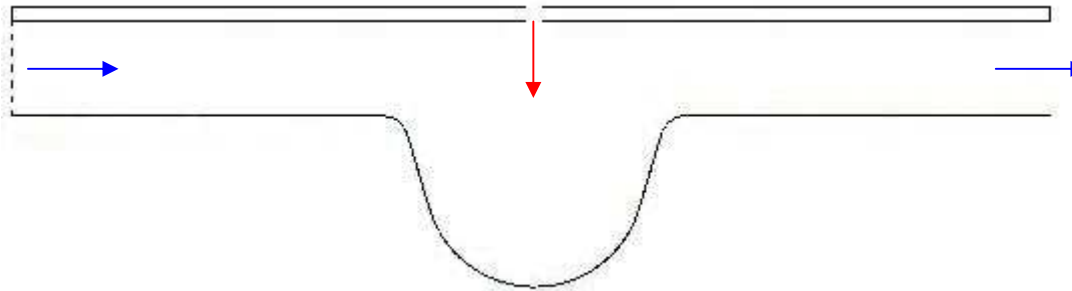
+ Chemical reaction + Kinetics Equation

F^{1-} / Nb^{5+} / NbF_5 concentration

Modeling Hypothesis

- Flow acid incoming (central cathode hole) non ideal

Dead end in beam pipe – non symmetric flow



- More intuitive solution
- Easier to model

Laminar flow through cavity from left to right

General Equations

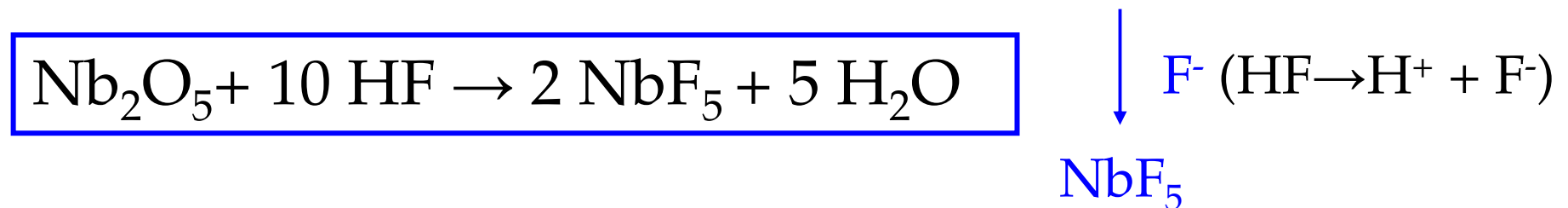
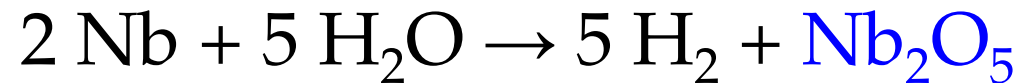
- Phenomenon transport (inspired from work of Lee et al.):

$$N_i = \underbrace{-D_i \nabla c_i}_{\text{Diffusion}} - \underbrace{z_i \cancel{\phi} F c_i}_{\text{Migration}} \nabla \phi + \underbrace{u c_i}_{\text{Convection}}$$

- Navier Stockes equation (incompressible fluid)
- Electroneutrality
- Gravity effect

Additional Equations

- Reminder of Nb electropolishing:



- Kinetic equation:

$$v = \frac{1}{2} \frac{d[\text{NbF}_5]}{dt} = k[\text{F}^-]^\alpha [\text{Nb}_2\text{O}_5]^\beta$$

→ Limit concentration in NbF₅

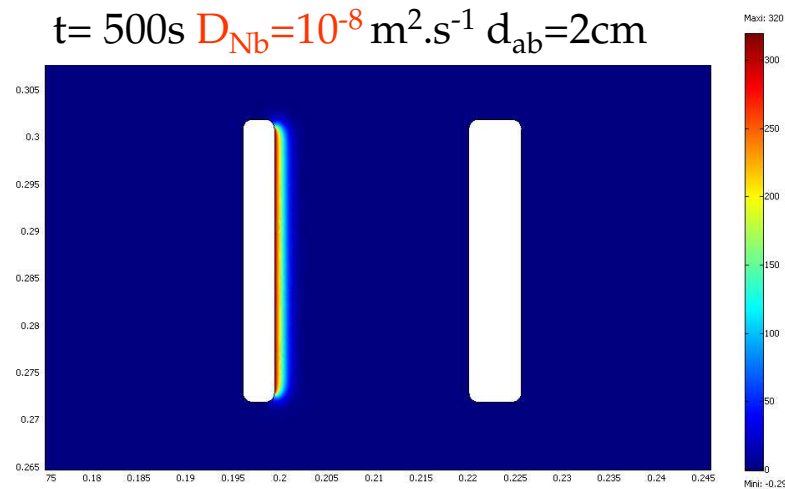
- Study of [F⁻]

Diffusion Coefficient

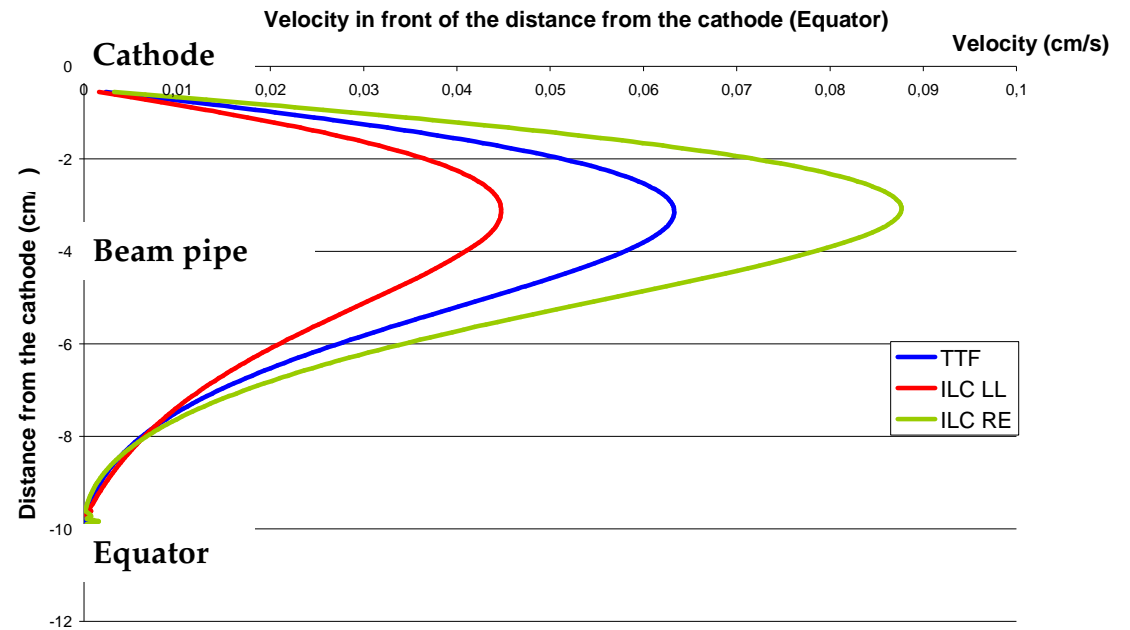
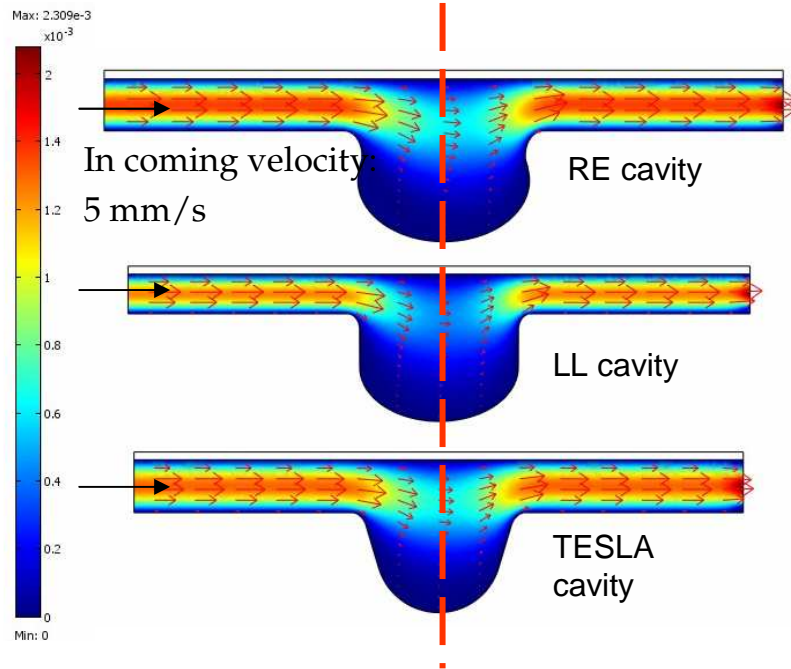
Determined from matching sample modeling
to experiments:

Fast forming of the viscous layer

Low density and high fluid viscosity to ensure its stability



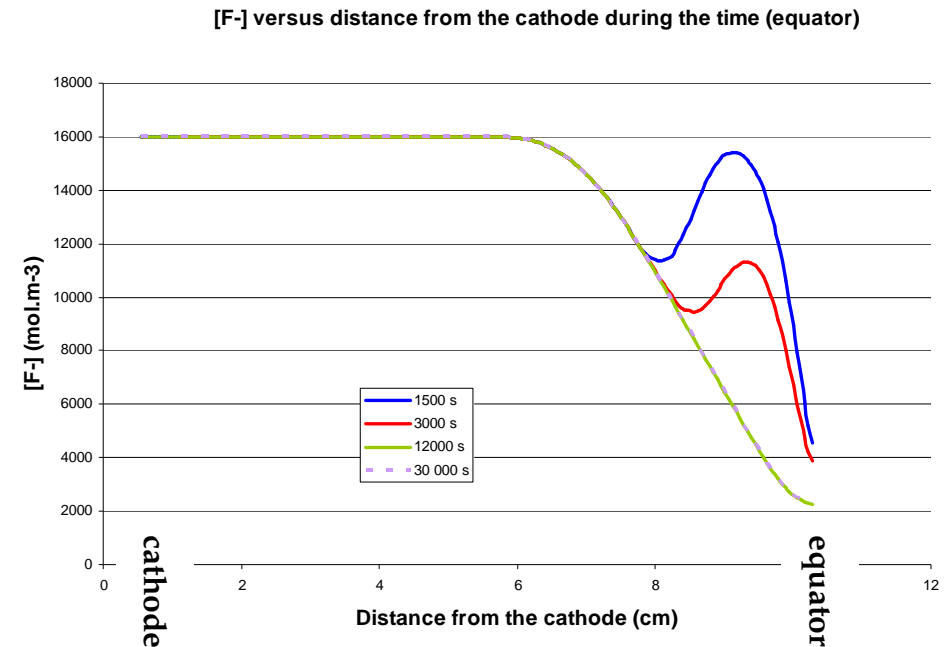
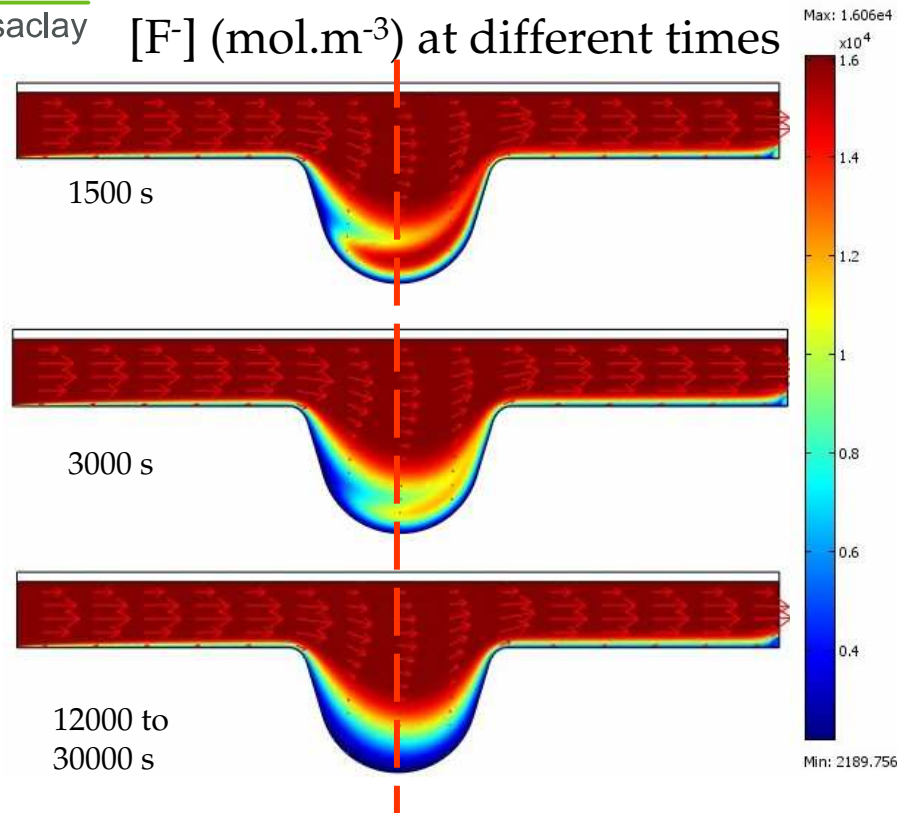
Fluid Velocity in the Cavity



For each cavity profile :

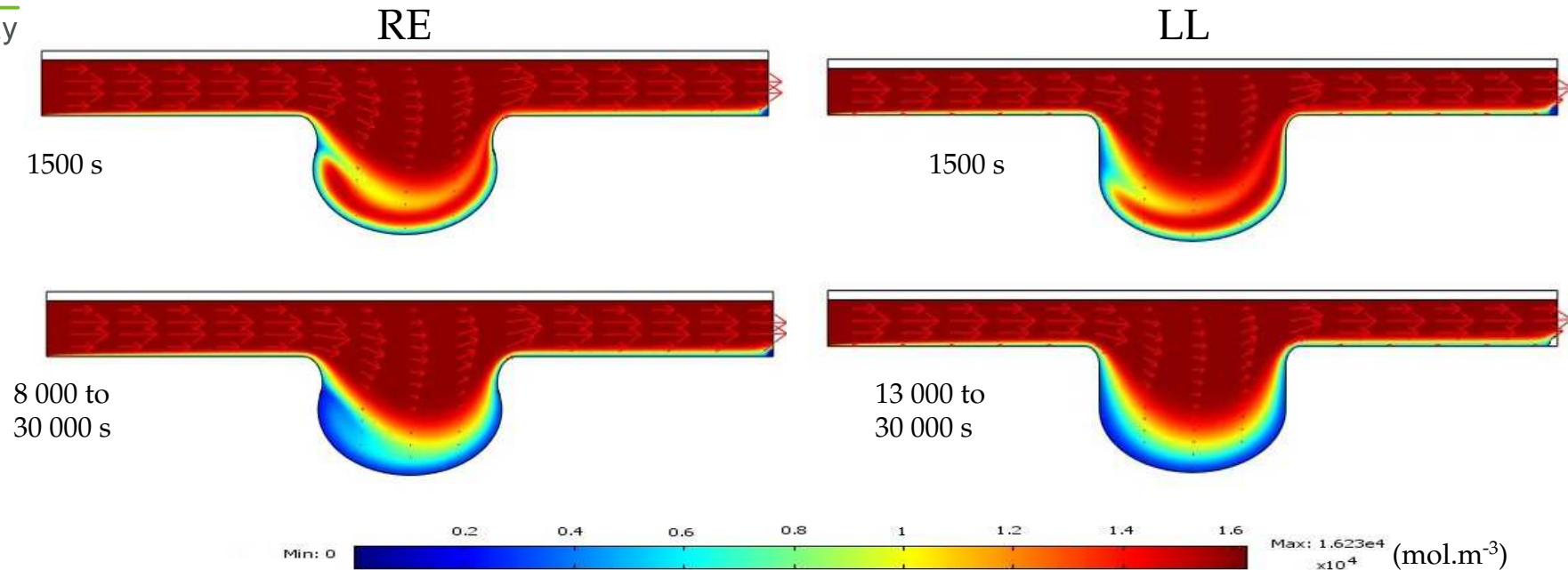
- Fluid velocity quasi null at the equator
- Highest velocity in the beam pipes

Bad Renewal of F^- at the Equator (TESLA shape)



- Before 12 000 s: $[F^-]$ decreases
- After 12 000 s: $[F^-]$ constant = bad regeneration of F^-
→ Aging of the acid at the equator

RE and LL Shapes

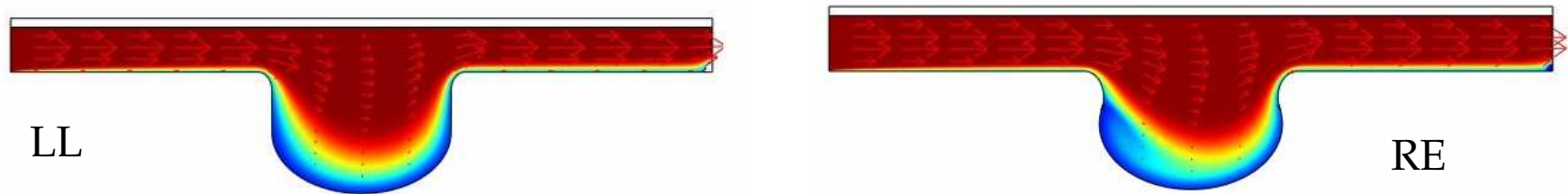


Same conclusions as for TESLA:

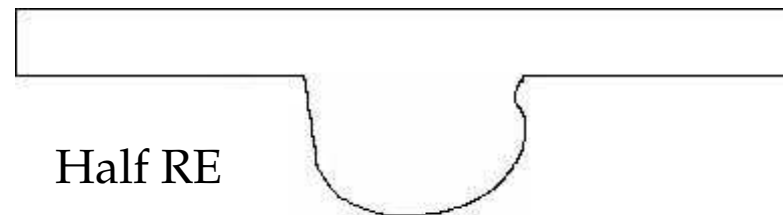
- Non uniform EP at the beginning
- Stabilization of the $[F^-]$ concentration after a long time
(cf. kinetics equation) → aging of the acid
- Not symmetric EP for the RE cavity

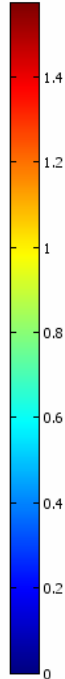
Half RE Shape

Not symmetric EP for the RE cavity

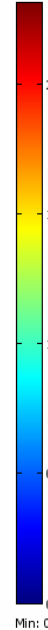
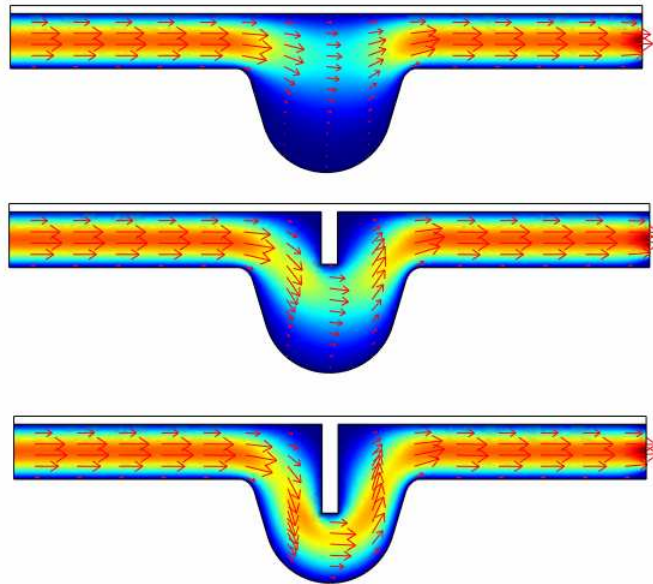


Half RE : interesting shape - outlook for the next modeling

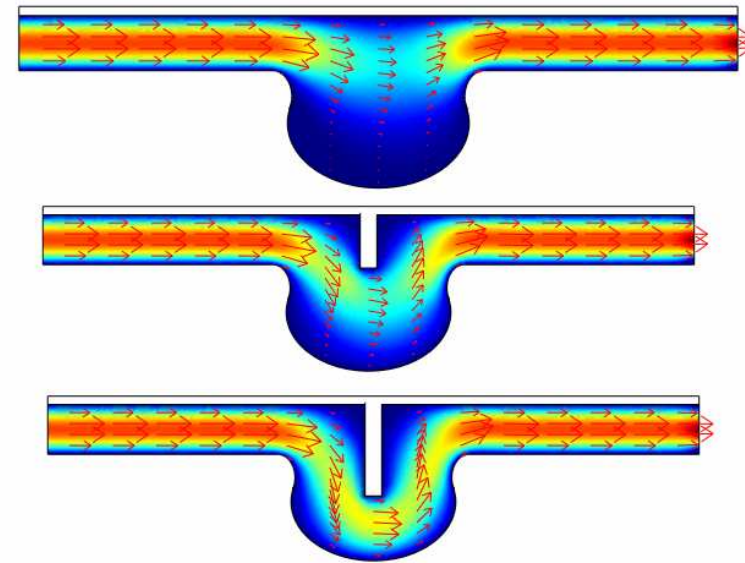




Fluid velocity for TESLA

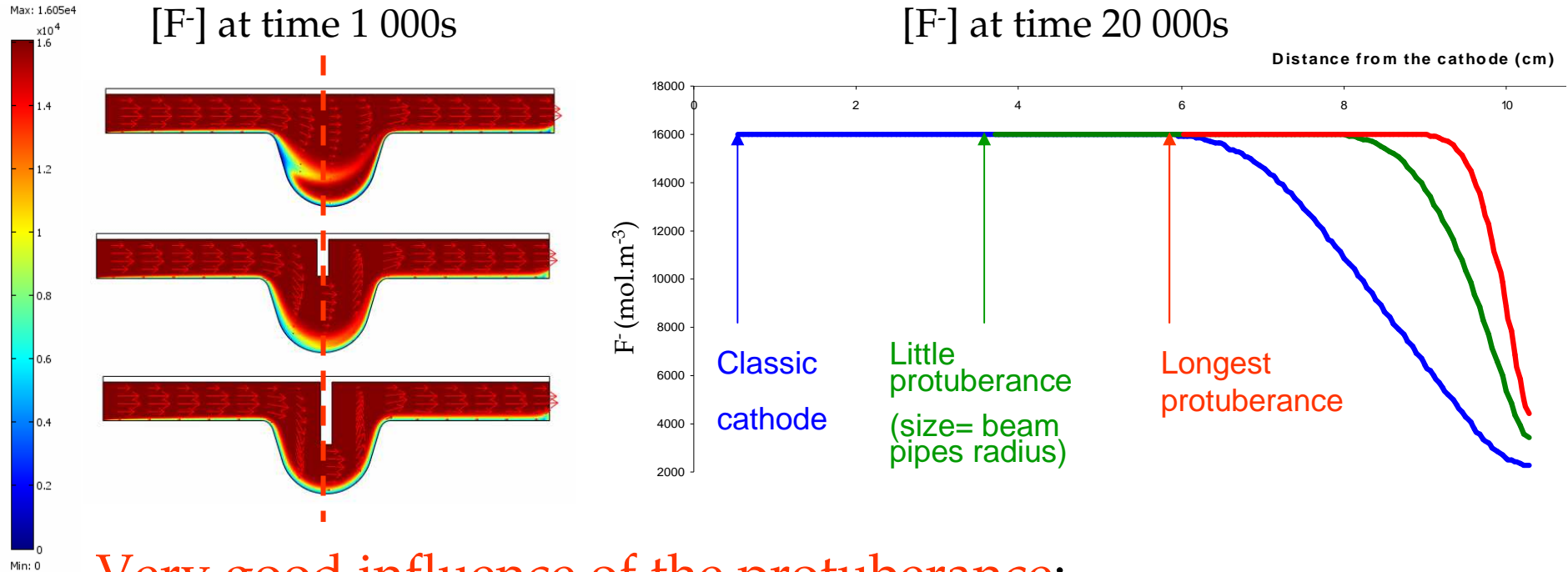


Fluid velocity for RE

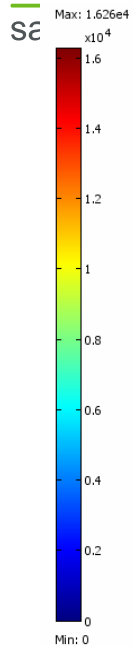
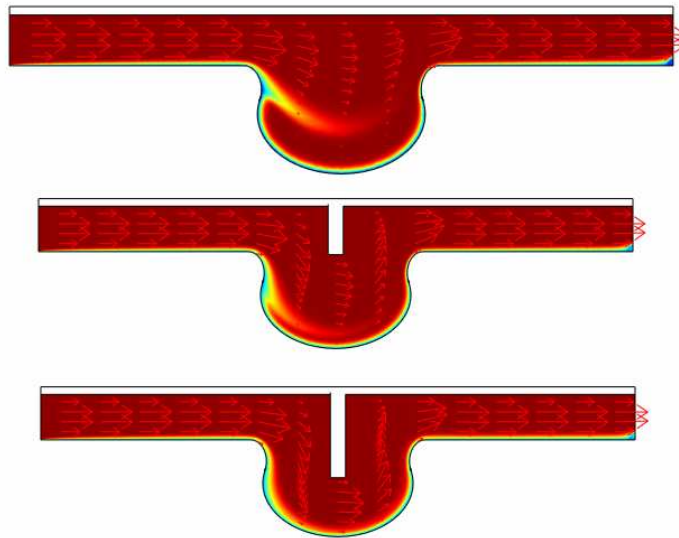


- Protuberance: force the acid to sweep the bottom of the cell for RE and TESLA → can extend this conclusion to LL
- Will it be enough to soften the asymmetric EP on RE ?
→ study the [F⁻] consumption

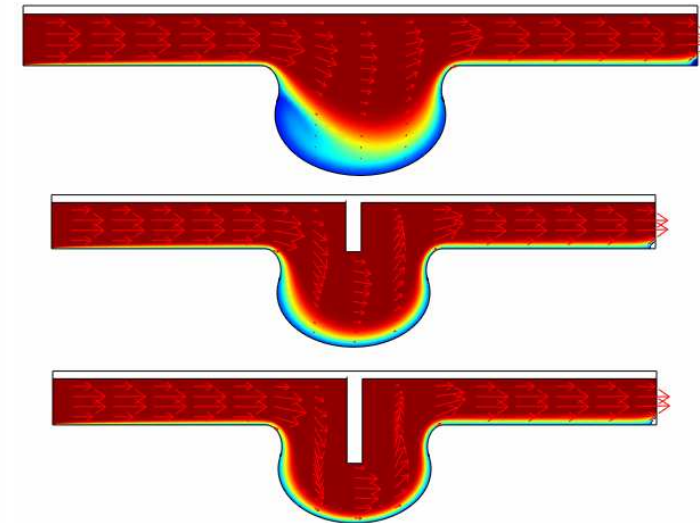
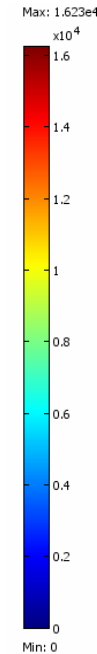
Adding a Protuberance (TESLA shape)



- Very good influence of the protuberance:
 - Reduce the perturbation in the cavity, faster stabilization
 - Better renewal of F⁻ at the equator (thinner and more concentrated layer of old acid) = **improved EP at the equator**

F⁻ at time 500s

(RE shape)

F⁻ at time 20 000s

- Same conclusion as for TESLA:
- Reduce the non uniform EP at the beginning and better renewal of the acid at the equator
- EP is more symmetric

Summary

- New acid incoming:
 - Can be applied for TESLA and LL shapes
 - **Asymmetric EP** in the cell for RE
 - Benefit effect of cathodic protuberance
- EP modeling well overcome:
 - Modeling central flow incoming to validate hypothesis
 - Model the more complex reality
(2D axi-symmetric, cavity rotation ...)

Thanks to ...

- Jacek Sekutowicz, Hasan Padamsee and Valery Shemelin to provide dimensions of cavity shape
- Bernard Visentin and Fabien Eozénou